

# ¿3ª generación de CSP?

## Avances y desafíos en ciclos de s-CO<sub>2</sub>



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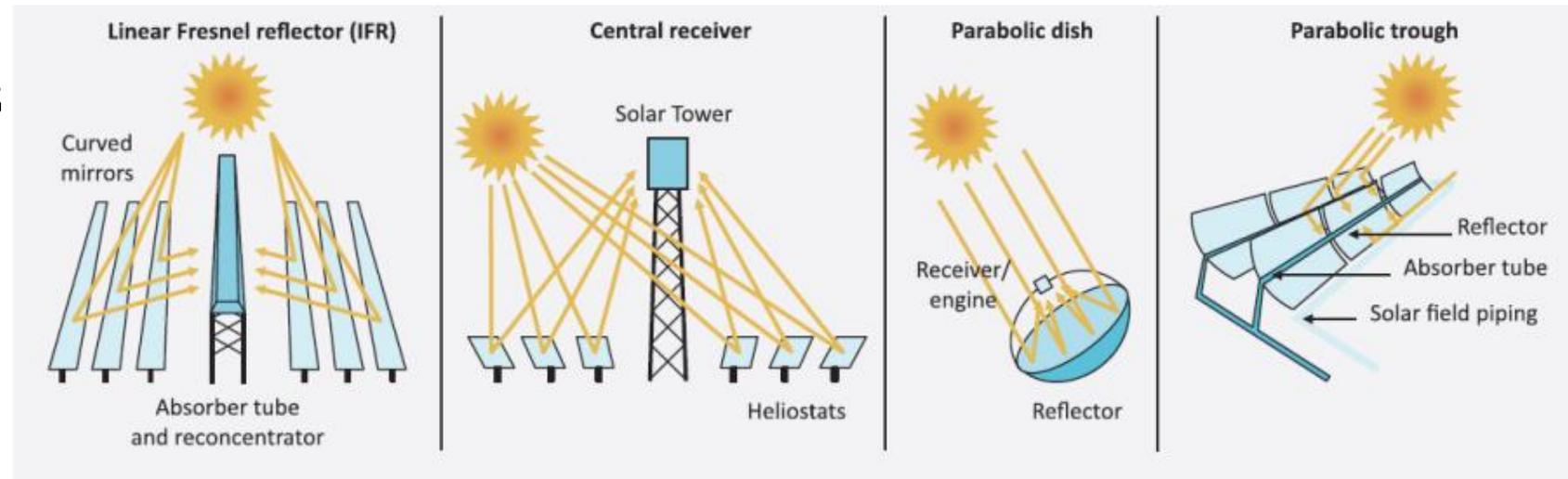
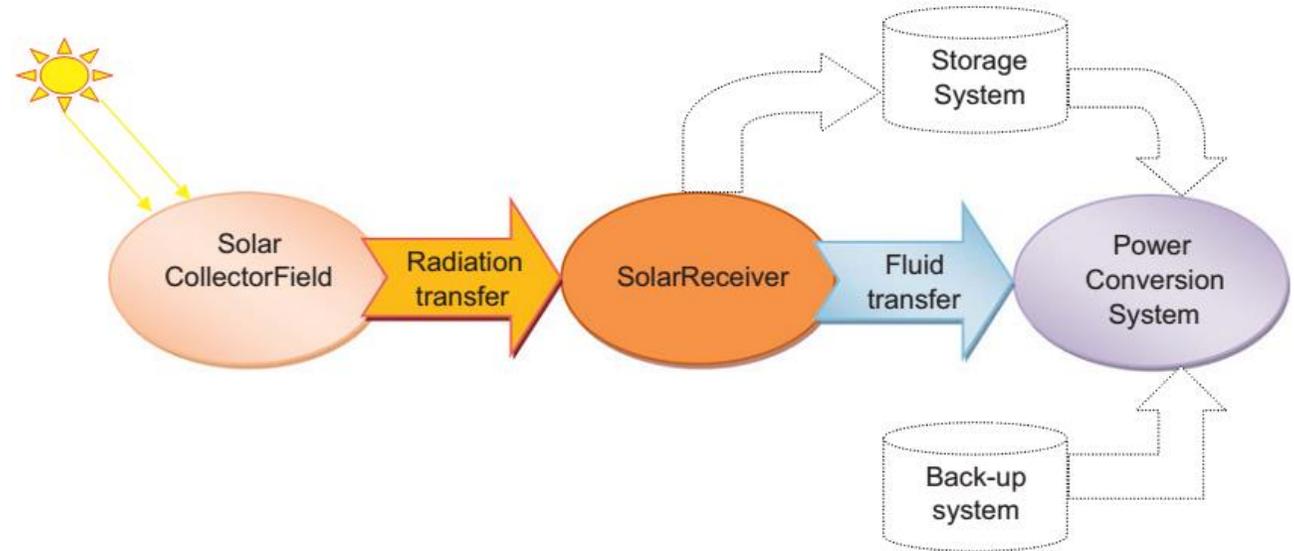
Santiago, 02/04/2018

José Miguel Cardemil

# Agenda

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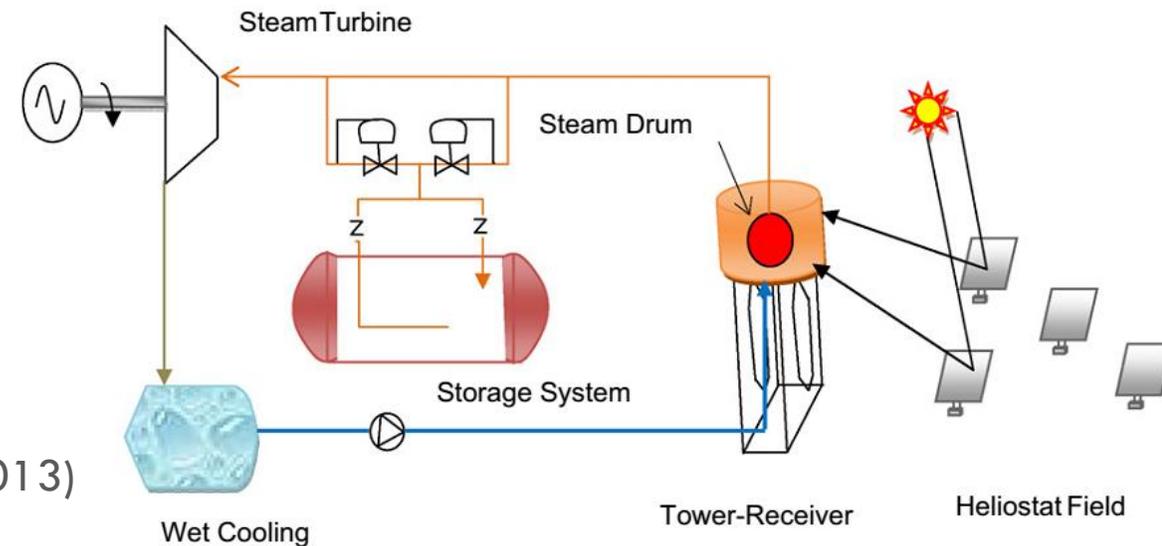
- ❑ Tecnología CSP
- ❑ Desafíos
- ❑ s-CO<sub>2</sub>
- ❑ Viabilidad Técnica
- ❑ Configuraciones
- ❑ Brechas Tecnológicas
- ❑ Otras alternativas



# Tecnologías CSP - Torre

3

- Primera Generación
  - ▣ Receptor opera con vapor saturado
- Abengoa
  - ▣ PS10
    - Construcción 2004-2007
    - Puesta en Marcha 2007
  - ▣ PS20
    - Construcción 2006-2009
    - Puesta en Marcha 2009
- Alta confiabilidad, pero bajo el umbral de la eficiencia comercial



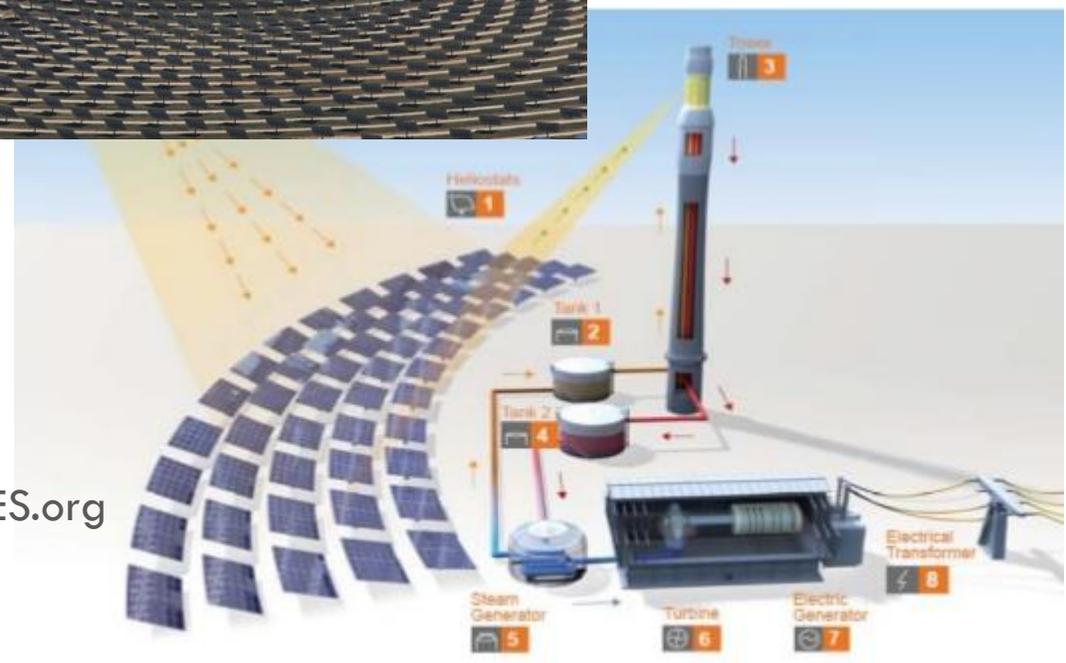
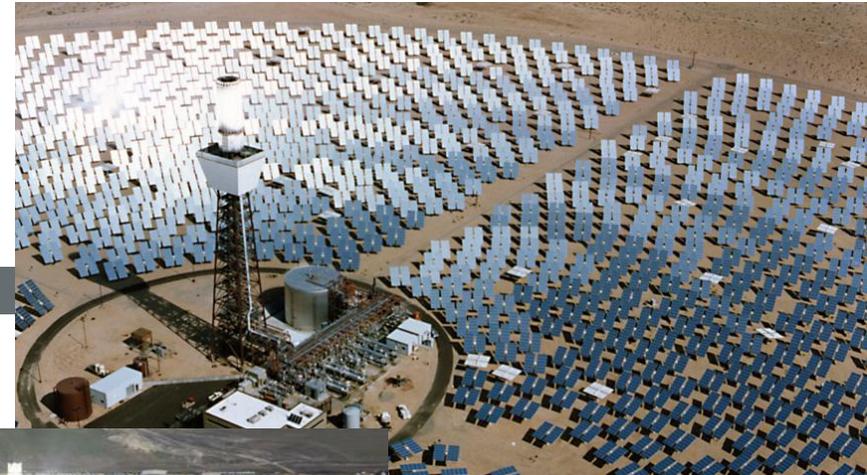
Fuente: Behar et. al. (2013)



# Tecnologías CSP - Torre

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- Segunda Generación
  - Receptor con sales fundidas
  - $\text{KNO}_3$  (40%) +  $\text{NaNO}_3$  (60%)
  - Solar Two
    - Nevada
  - Gemasolar
    - Sevilla
- Facilidad de integración
  - Almacenamiento térmico
  - Back Up



Fuente: SolarPACES.org

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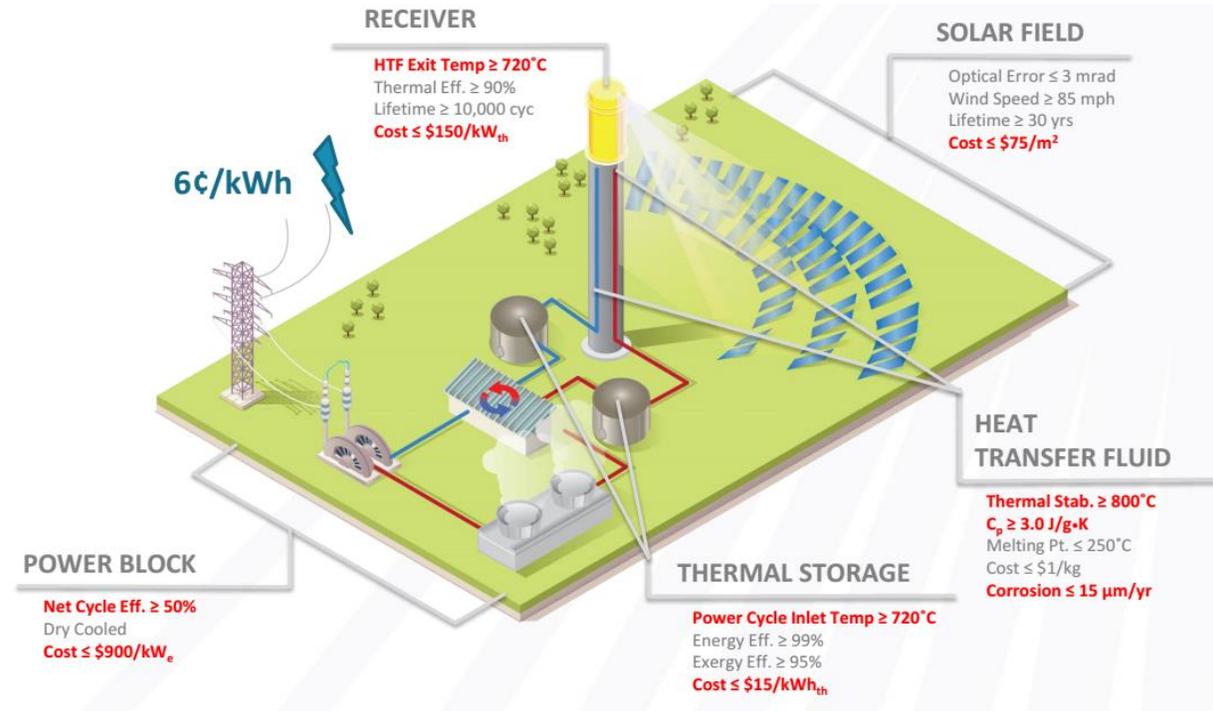
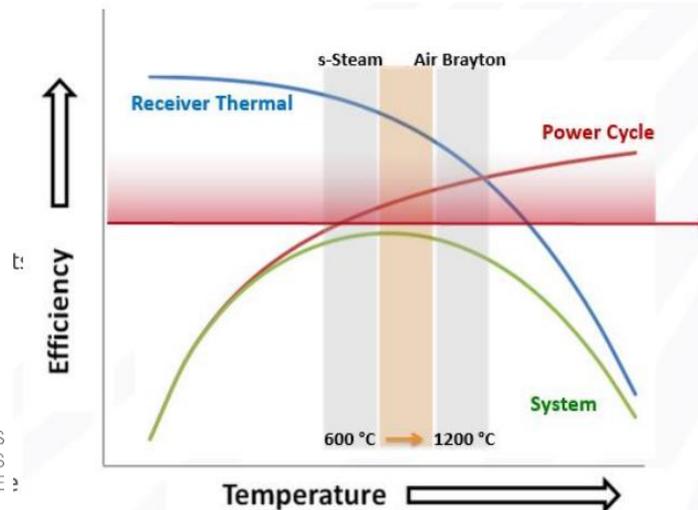
# Desafíos

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- Reducir costos
  - ▣ Hibridación CSP+PV
    - Escala
- Aumentar eficiencia de conversión

→ Aumentar temperaturas de operación

$$\eta = 1 - \frac{T_L}{T_H}$$

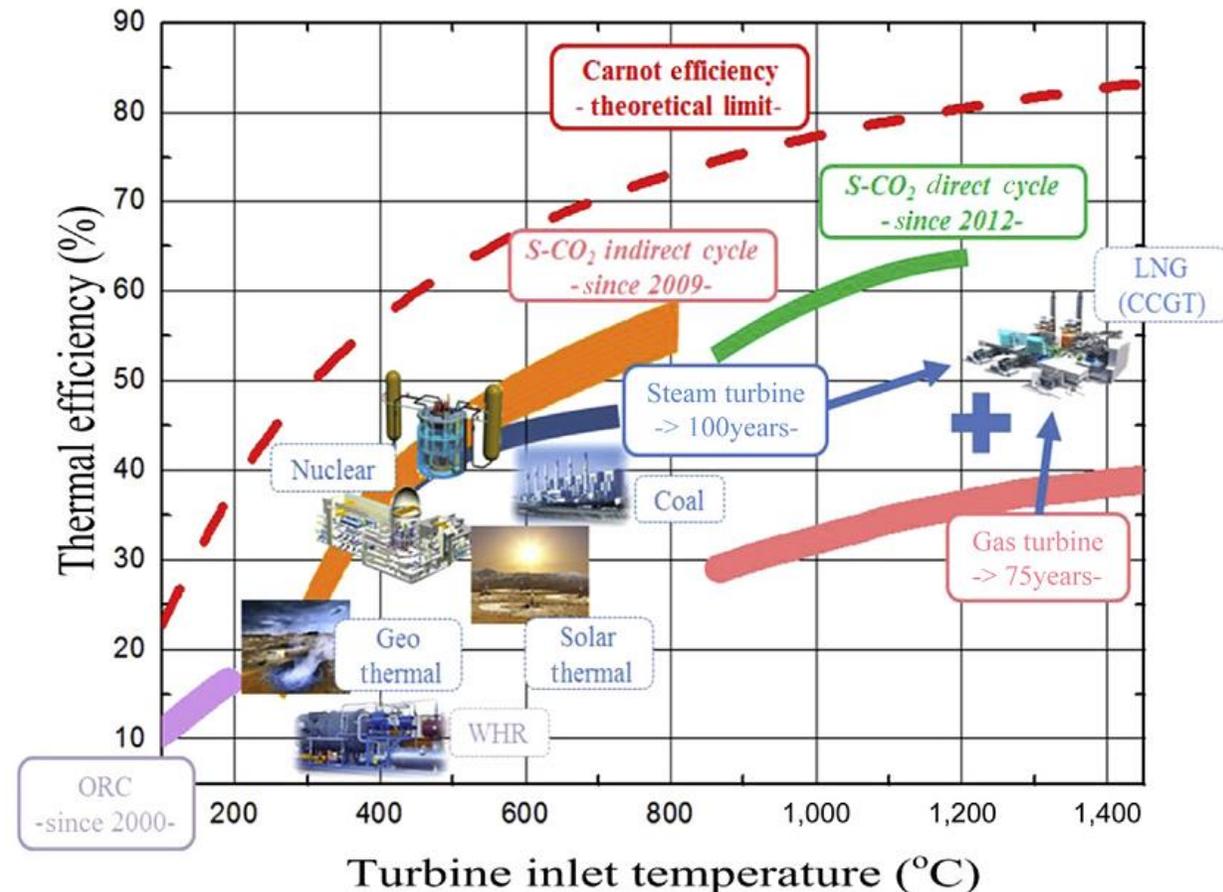


Fuente: [energy.gov/sunshot](http://energy.gov/sunshot)

# CO<sub>2</sub> como Fluido de Trabajo

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- Fluidos de trabajo comúnmente usados en ciclos térmicos
  - Butane, R11, Ammonia, pentane, Isopentane, Isobutene, Toluene, Hydrocarbon mixtures, other fluids.
  - Desventajas
    - Inflamables, altamente tóxicos, elevado GWP, afectan la capa de ozono y elevado costo.
- CO<sub>2</sub> no presenta las desventajas mencionadas, pero...
  - Propiedades altamente variables
  - Altas presiones de operación



Fuente: Ahn et. al. (2015)



# CO<sub>2</sub> como Fluido de Trabajo

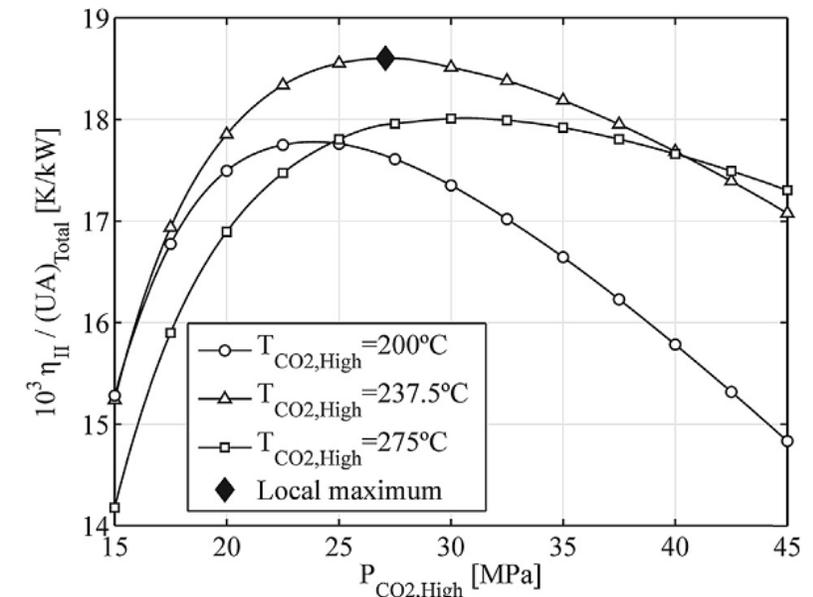
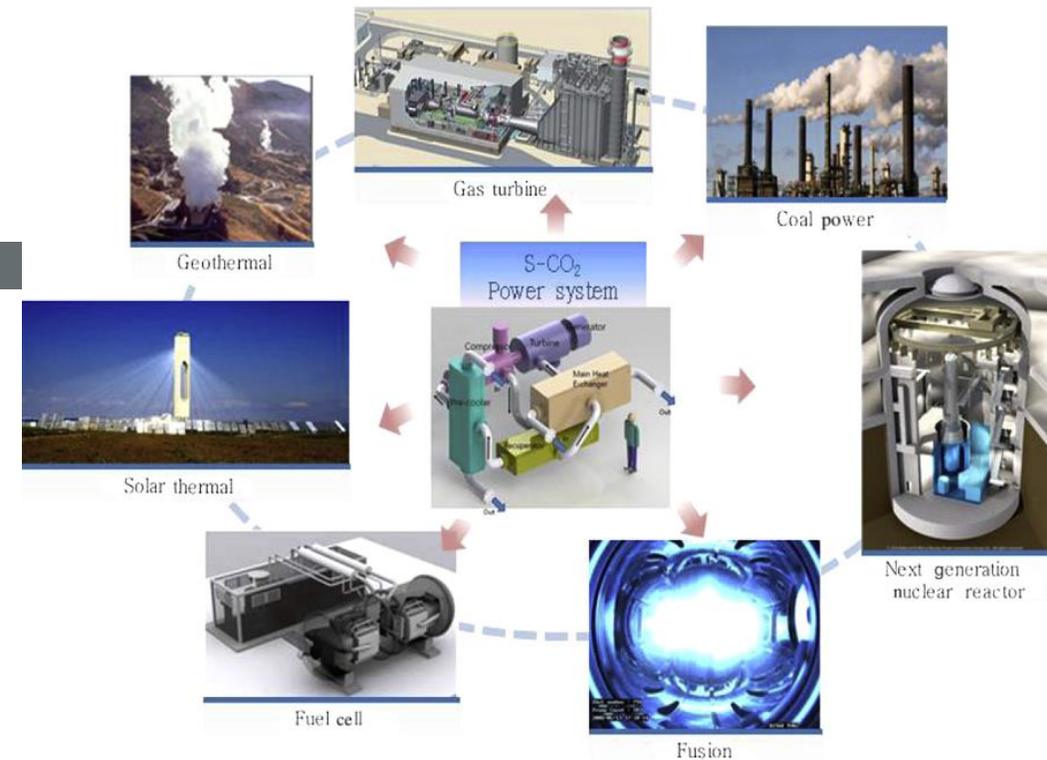
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□ Inicialmente investigado para ser utilizado en centrales nucleares

■ Angelino et al. (1968)

□ Varios autores han demostrado las ventajas del uso de CO<sub>2</sub> y optimizado sus condiciones de operación

- Battisti, F. G., Cardemil, J. M., & Da Silva, A. K. (2016). A multivariable optimization of a Brayton power cycle operating with CO<sub>2</sub> as working fluid. *Energy*, 112, 908–916.
- Cardemil, J. M., & da Silva, A. K. (2016). Parametrized overview of CO<sub>2</sub> power cycles for different operation conditions and configurations – An absolute and relative performance analysis. *Applied Thermal Engineering*, 100, 146–154.

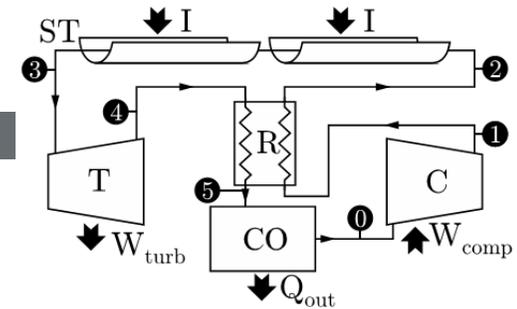


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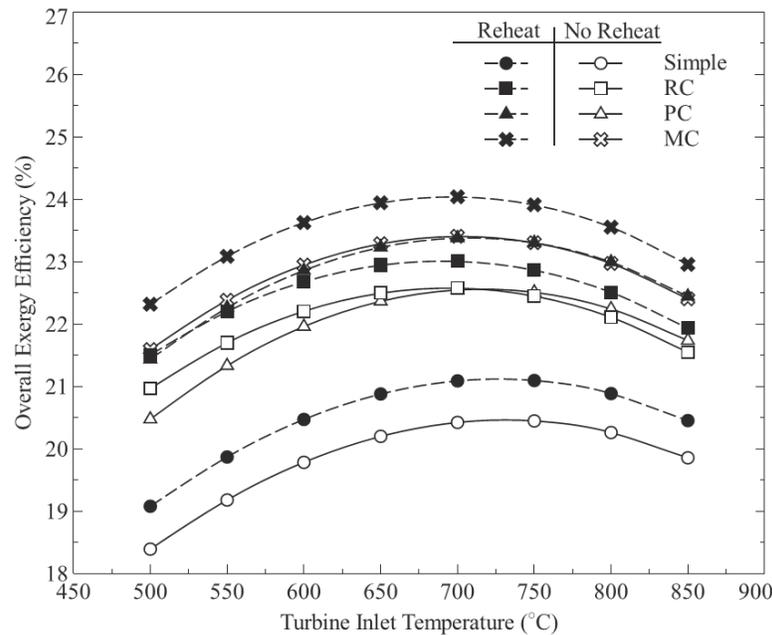
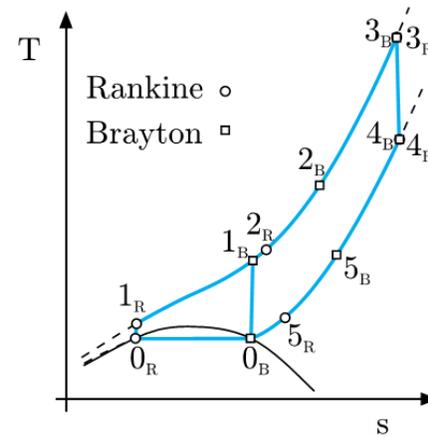
# CO<sub>2</sub> como Fluido de Trabajo en CSP

## Algunos autores han analizado su utilización en concentradores lineales

de Araujo Passos, L. A., de Abreu, S. L., & da Silva, A. K. (2017). Optimal scale of solar-trough powered plants operating with carbon dioxide. *Applied Thermal Engineering*, 124, 1203–1212.

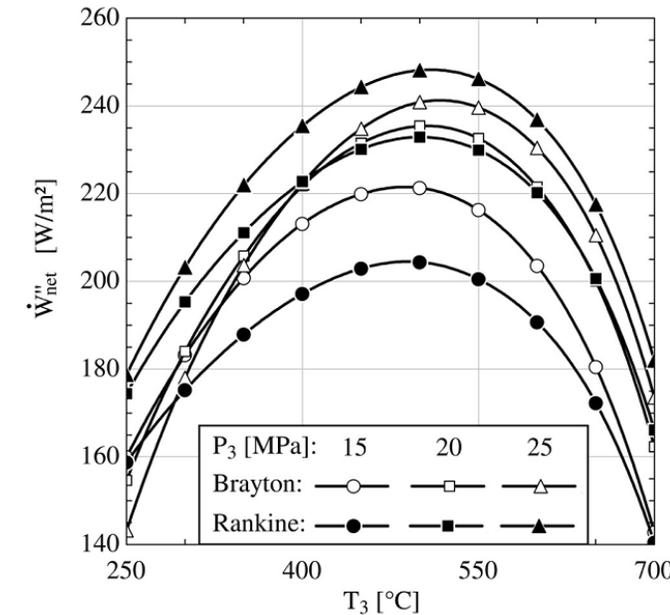


C=Compressor  
CO=Cooler  
R=Recuperator  
ST=Solar Trough  
T=Turbine



## Pero su mejor desempeño se observa en sistemas de torre

Padilla, R. V., Soo Too, Y. C., Benito, R., & Stein, W. (2015). Exergetic analysis of supercritical CO<sub>2</sub> Brayton cycles integrated with solar central receivers. *Applied Energy*, 148, 348–365.



# Pero Cuales son los desafíos pendientes

## Almacenamiento Térmico

### Química de sales

Salt	Composition by Wt.	Melting Point (°C)	Heat Capacity (J/g-K)	Density (kg/L)	Δ Volume on Melting	Notes**	Ref.
NaNO <sub>3</sub> KNO <sub>3</sub> (baseline)	0.60 0.40	220	1.52	1.7	+4.6%		[10]
ZnCl <sub>2</sub> NaCl KCl	0.686 0.075 0.239	204	0.81	2.4	NaCl/KCl: +14.8% [11] NaCl: +26.1% KCl: +22.3% [11]	ZnCl BP(732°C) [12]	[13]
MgCl <sub>2</sub> KCl	0.375 0.625	426	1.15	1.66	KCl: +22.3% MgCl <sub>2</sub> : +30.5% [11]	MgCl <sub>2</sub> BP(1412°C)	[14]
Na <sub>2</sub> CO <sub>3</sub> K <sub>2</sub> CO <sub>3</sub> Li <sub>2</sub> CO <sub>3</sub>	0.334 0.345 0.321	398	1.61	2.0	+3.6% [11]	EP(747°C) 0.014 atm EP(827°C) 0.041 atm EP(947°C) 0.151 atm [9] [12]	[13] [15]

\*\*BP(XXX°C): boiling point temperature, EP(XXX°C): equilibrium pressure at a given temperature of CO<sub>2</sub>

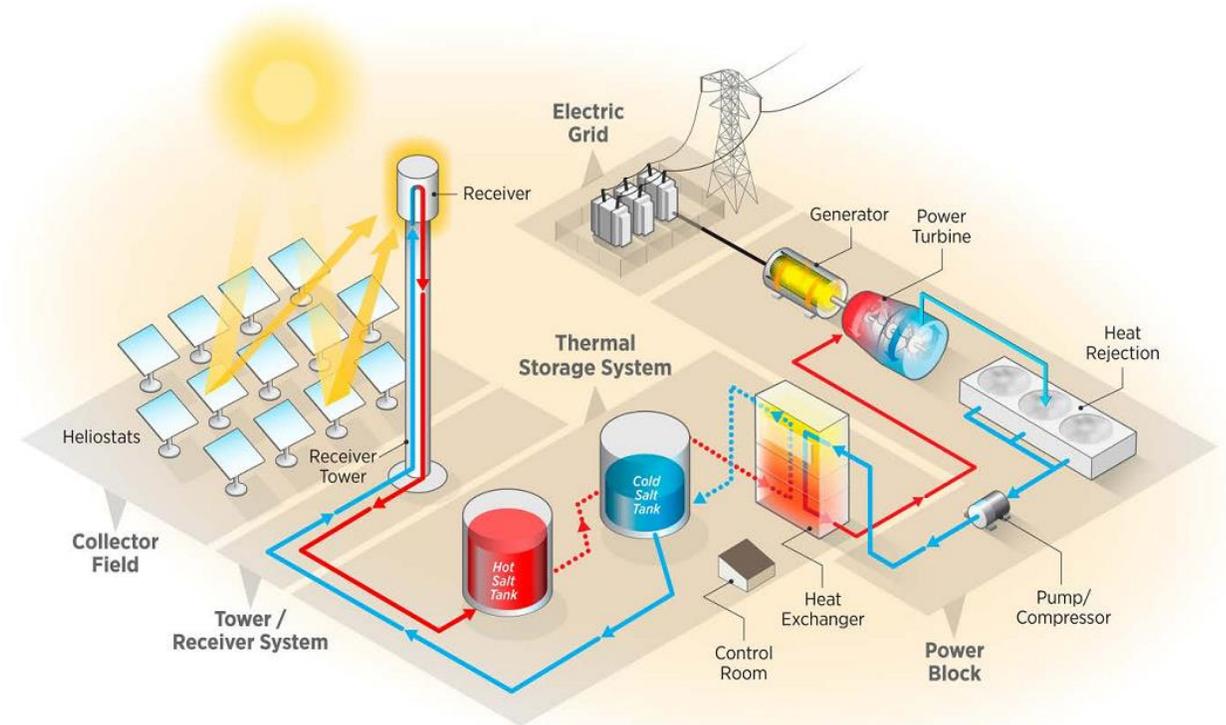
Salt	Notable Advantages	Notable Disadvantages
Zn-based chloride	<ul style="list-style-type: none"> <li>Lowest melting point</li> <li>Corrosion mitigation via control of melt redox potential (oxygen and water exclusion) in inert atmospheres</li> </ul>	<ul style="list-style-type: none"> <li>Measureable vapor pressure disperses ZnCl<sub>2</sub> in headspace</li> <li>Very corrosive in liquid and vapor phases if oxygen or water exist. Intergranular corrosion can occur.</li> <li>Lowest heat capacity</li> <li>Requires controlled purification and pre-melting procedures under vacuum</li> </ul>
Mg-based chloride	<ul style="list-style-type: none"> <li>Lowest cost per kg</li> <li>Corrosion mitigation via control of melt redox potential using active-metals such as Mg in inert atmospheres with oxygen/water exclusion</li> </ul>	<ul style="list-style-type: none"> <li>Highest melting point</li> <li>Very corrosive in liquid and vapor phases if oxygen or water exist. Intergranular corrosion can occur.</li> <li>Intergranular corrosion if Mg concentration decreases below required value</li> <li>Requires controlled purification and pre-melting procedures under inert atmospheres</li> </ul>
Ternary carbonate eutectic	<ul style="list-style-type: none"> <li>High heat capacity and density leads to smallest required tank volume</li> <li>Does not require controlled purification and pre-melting procedures.</li> <li>Inherently compatible with CO<sub>2</sub></li> <li>Substantial experience from use in molten-carbonate fuel cells (Li/K carbonates) operating at ~650°C</li> </ul>	<ul style="list-style-type: none"> <li>Highest cost per kg (unless low-Li blends are proven effective)</li> <li>High melting point</li> <li>Lithium is a critical metal for many applications, especially batteries, which will affect market prices</li> </ul>



# Desafíos pendientes: s-CO<sub>2</sub> + Sales

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- Combatividad de materiales/sales
  - Corrosión
  - Bombas
  - Válvulas
  - Piping
  - Receptor
  - Intercambiadores de calor
    - Micro canales pre-impresos



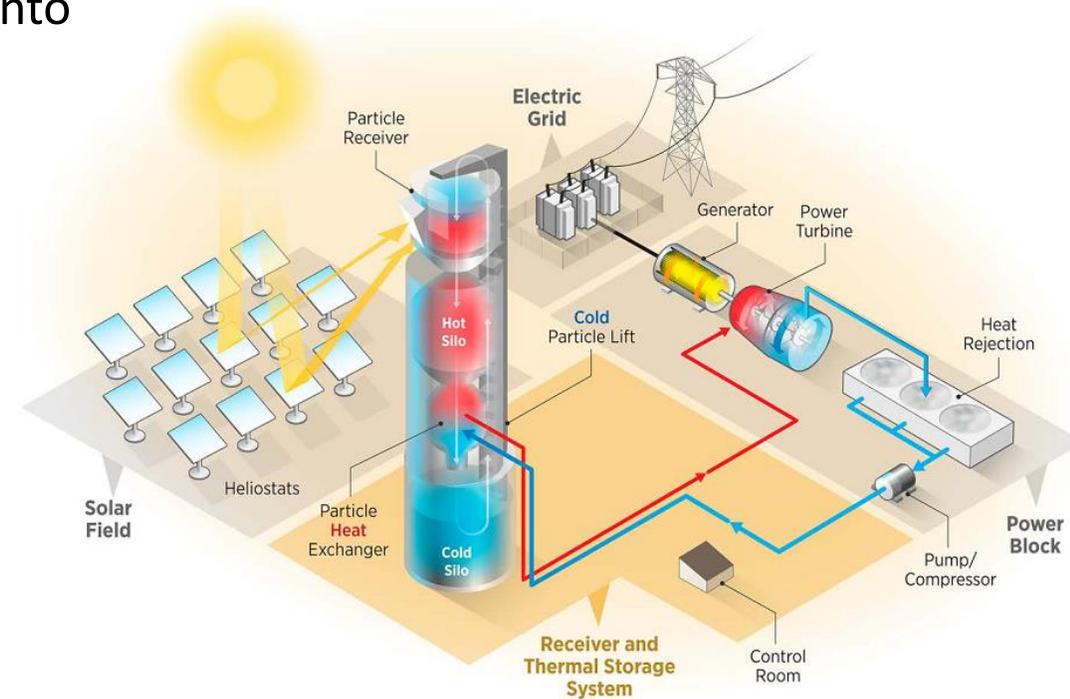
Fuente: SAM (2017)



# Otra alternativa: Falling Particles

- ❑ Partículas sólidas absorben la radiación: Directa o indirectamente
- ❑ Las propias partículas actúan como medio de almacenamiento
- ❑ Desafíos:
  - ❑ Resistencia de las partículas (pérdida)
  - ❑ Geometría del receptor
  - ❑ Almacenamiento de partículas
  - ❑ Intercambiador de calor

Material	Composition	Properties <sup>a</sup>		Advantage	Disadvantage
		Density(kg/m <sup>3</sup> )	Specific Heat (J/kg-K)		
Silica sand	SiO <sub>2</sub>	2,610	1,000	Stable, abundant, low cost	Low solar absorptivity and conductivity
Alumina	Al <sub>2</sub> O <sub>3</sub>	3,960	1,200	Stable	High cost
Coal ash	SiO <sub>2</sub> , Al <sub>2</sub> O <sub>3</sub> , + minerals	2,100	720 at ambient temperature	Stable, abundant, No/low cost	Identify suitable ash
Calcined Flint Clay	SiO <sub>2</sub> , Al <sub>2</sub> O <sub>3</sub> , TiO <sub>2</sub> , Fe <sub>2</sub> O <sub>3</sub>	2,600	1,050	Mined, abundant, used as filler in FB boiler	Low absorptivity
Ceramic proppants	75% Al <sub>2</sub> O <sub>3</sub> , 11% SiO <sub>2</sub> , 9% Fe <sub>2</sub> O <sub>3</sub> , 3% TiO <sub>2</sub>	3,300	1,200 (at 700°C)	High solar absorptivity, stable	Synthesized, higher cost



C. Ho et al., "Technology advancements for next generation falling particle receivers," in *Proceedings of the Solarpaces 2013 International Conference (Energy Procedia)*, 2014.



# Fase gaseosa: Receptor de cavidad

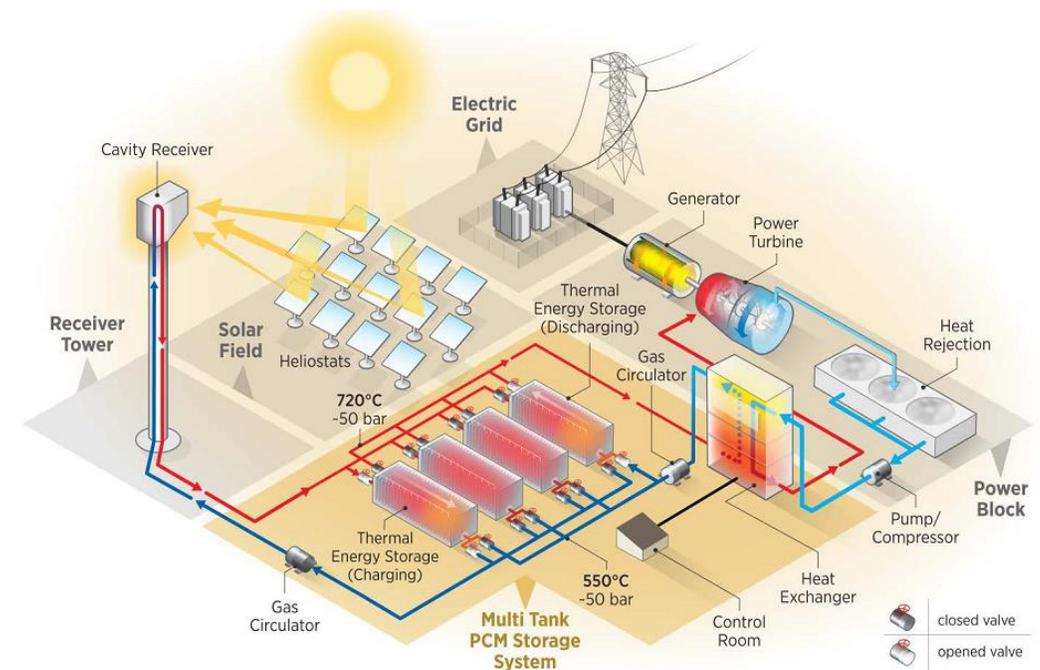
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## □ El gas absorbe calor directamente en el absorbedor

- Receptor volumétrico/cavidad
- Absorbedor → Medio Poroso
- Apto para CO<sub>2</sub>, Helio y Aire
- Estabilidad y altas efectividad de absorción
- Bajo costo e impacto ambiental

## □ Desafíos

- Capacidad de transferencia de calor reducida
- Integración a TES
- Alta potencia en flujo de fluidos → Complejidad en el patrón de flujo



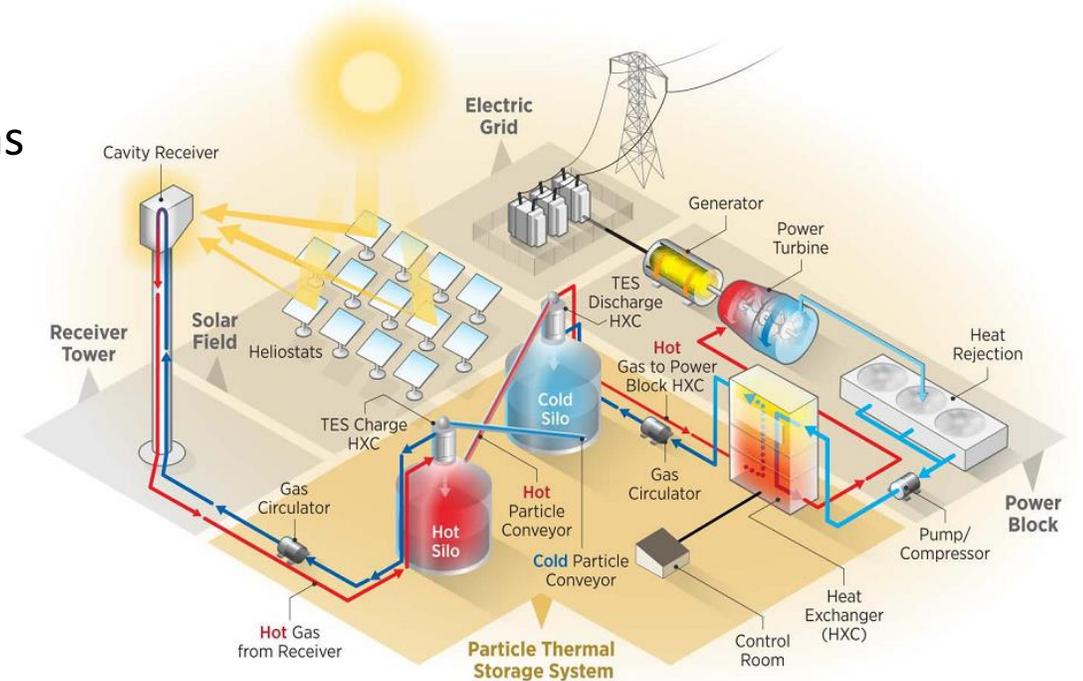
Fuente: NREL (2017)



# Una combinación de las alternativas anteriores?

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- Substituir la configuración de convencional de dos tanques, por dos silos
- Receptor volumétrico + almacenamiento en partículas
- Aún en estudio, muchos desafíos en relación a la integración y al sistema de control



Fuente: NREL (2017)



# Opciones Tecnológicas

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	Collector Field		
	<ul style="list-style-type: none"> <li>• Cost &lt;\$75/m<sup>2</sup></li> <li>• Concentration ratio &gt;50</li> </ul>	<ul style="list-style-type: none"> <li>• Operable in 35-mph winds</li> </ul>	<ul style="list-style-type: none"> <li>• Optical error &lt;3.0 mrad</li> <li>• 30-year lifetime</li> </ul>
	Molten Salt	Falling Particle	Gas Phase
Receiver	<ul style="list-style-type: none"> <li>• Similarities to prior demonstrations</li> <li>• Allowance for corrosive attack required</li> </ul>	<ul style="list-style-type: none"> <li>• Most challenging to achieve high thermal efficiency</li> </ul>	<ul style="list-style-type: none"> <li>• High-pressure fatigue challenges</li> <li>• Absorptivity control and thermal loss management</li> </ul>
Material & Support	<ul style="list-style-type: none"> <li>• Potentially chloride or carbonate salt blends; ideal material not determined</li> <li>• Corrosion concerns dominate</li> </ul>	<ul style="list-style-type: none"> <li>• Suitable materials readily exist</li> </ul>	<ul style="list-style-type: none"> <li>• Minimize pressure drop</li> <li>• Corrosion risk retirement</li> </ul>
Thermal Storage	<ul style="list-style-type: none"> <li>• Direct or indirect storage may be superior</li> </ul>	<ul style="list-style-type: none"> <li>• Particles likely double as efficient sensible thermal storage</li> </ul>	<ul style="list-style-type: none"> <li>• Indirect storage required</li> <li>• Cost includes fluid to storage thermal exchange</li> </ul>
HTF to sCO <sub>2</sub> Heat Exchanger	<ul style="list-style-type: none"> <li>• Challenging to simultaneously handle corrosive attack and high-pressure working fluid</li> </ul>	<ul style="list-style-type: none"> <li>• Possibly greatest challenge</li> <li>• Cost and efficiency concerns dominate</li> </ul>	<ul style="list-style-type: none"> <li>• Not applicable</li> </ul>
Supercritical CO <sub>2</sub> Brayton Cycle			
	<ul style="list-style-type: none"> <li>• Net thermal-to-electric efficiency &gt; 50%</li> </ul>	<ul style="list-style-type: none"> <li>• Power-cycle system cost &lt; \$900/kW<sub>e</sub></li> </ul>	<ul style="list-style-type: none"> <li>• Dry-cooled heat sink at 40° C ambient</li> <li>• Turbine inlet temperature ≥ 700°C</li> </ul>

**Receiver**  
*Cost < \$150/kWth*  
*Thermal Efficiency > 90%*  
*Exit Temperature > 720°C*  
*10,000 cycle lifetime*

**Material & Support**  
*Cost < \$1/kg*  
*Operable range from 250°C to 800°C*

**Thermal Storage**  
*Cost < \$15/kW<sub>th</sub>*  
*99% energetic efficiency*  
*95% exergetic efficiency*

**HTF to sCO<sub>2</sub> Heat Exchanger**

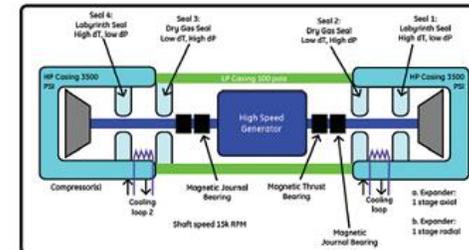
Fuente:  
 NREL 2017, Concentrating Solar Power Gen3 Demonstration Roadmap

# Un desafío adicional...

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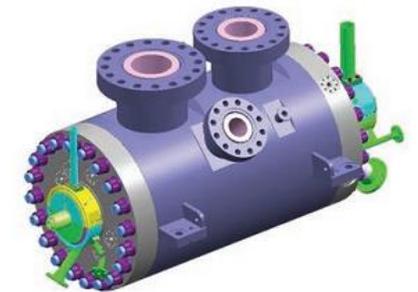
- Turbinas de CO<sub>2</sub> con elevadas eficiencias aun no están disponibles
- Programa SunShot ha investido significativos recursos en este tópico
  - 2020 Operación de pilotos
  - 2030 Escala comercial

<b>SOUTHWEST RESEARCH INSTITUTE</b>	
PROGRAM:	SunShot CSP R&D 2012
TOPIC:	Advanced Power Cycles
LOCATION:	San Antonio, Texas
AWARD AMOUNT:	Up to \$6.8 million
PROJECT TERM:	2012–2015



Conceptual layout of an integrated, high-efficiency supercritical CO<sub>2</sub> hot gas turbo-expander that is optimized for the highly transient solar power plant duty cycle profile. Illustration from Southwest Research Institute

<b>NATIONAL RENEWABLE ENERGY LABORATORY</b>	
PROGRAM:	SunShot CSP R&D 2012
TOPIC:	Advanced Power Cycles
LOCATION:	Golden, Colorado
AWARD AMOUNT:	Up to \$8 million
PROJECT TERM:	2012–2015



This project's team will build a prototype of the largest and highest-temperature s-CO<sub>2</sub> closed Brayton power cycle turbine ever constructed. The use of carbon dioxide instead of steam allows higher power-cycle efficiency and more compact cycle components. Illustration from Dresser-Rand



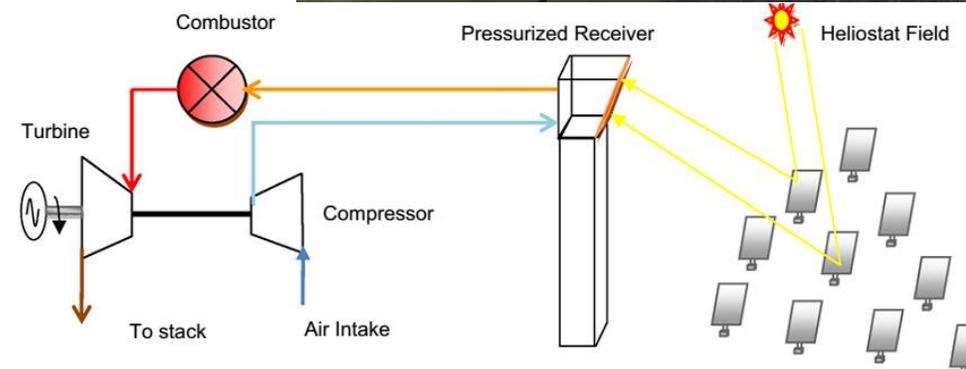
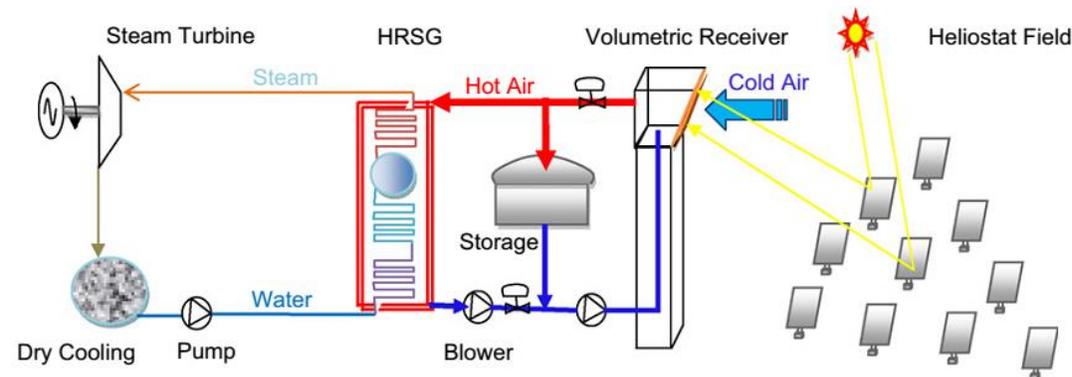
# Pero es el CO<sub>2</sub> la única alternativa?

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- Una alternativa:
  - ▣ Aire atmosférico como fluido de trabajo
    - Barato y estable
    - Fácil de integrar con ciclos de gas
- Desafíos:
  - ▣ Receptor volumétrico
  - ▣ Almacenamiento térmico costo efectivo
    - Rocas?
    - Concreto?
- Proyecto en evaluación



Fuente: CSP 247 (2018)



Santiago, 02/04/2018



# Muchas Gracias



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